

## Going with the Flow – The Use of Continuous Processing in Organic Synthesis

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## Continuous Processing – A Hot Topic in Both Industry and Academia

### GOING WITH THE FLOW

Continuous reactors arrive in the drug industry P.13

HEMICAL & ENGINEERING NEWS

Thayer, A. M. *Chem. Eng. News* **2014**, 92 (21), p. 13

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funding models **P.27** 

### **PROS AND CONS**

Continuous processes have advantages over batch methods, but they have challenges as well.

#### Advantages

- Low capital investment
- Less space required
- Safer with hazardous reactions
- Shorter processing times
- Possible novel chemistries
- Straightforward scale-up
- Need for less inventory
- Potential cost savings
- Better product quality
- Improved environmental impact

### Challenges

- Competes with existing investments
- Mind-set change needed to shift
- Perception of higher risk
- New engineering/operating skills
- Lack of adequately trained people
- Equipment availability at all scales
- Up-front development demands
- Limitations with solids
- Mastery of start-up and shutdown
- Relatively untested regulatory path





## **Continuous Processing has Arrived in Big Pharma**

### Novartis to give MIT \$65m to find new way to produce drugs Focus on manufacturing

The Boston Blobe

By Todd Wallack, Globe Staff | September 28, 2007

Drug giant <u>Novartis</u> AG says it will give its Cambridge neighbor, MIT, \$65 million over 10 years to create a research program, likely to be the biggest in the world aimed at revolutionizing the way drugs are made.

The goal is to help companies move from making drugs in batches to using a continuous high-tech process that will save time and money.

### **GSK** commits to continuous processing

Witty says it could be used on up to half of the company's drugs

February 19, 2013 | By Eric Palmer

### The Mainstreaming of Continuous Flow API Synthesis

The pharma industry is moving toward commercial-scale continuous processes for small-molecule API manufacturing.

Jul 02, 2014 By Cynthia A. Challener Pharmaceutical Technology Volume 38, Issue 7

# Vertex, J&J, GSK, Novartis all working on continuous manufacturing facilities

FDA supports the move as a way to improve quality in manufacturing

February 9, 2015 | By Eric Palmer

## Lilly takes to continuous manufacturing with \$40m Irish investment

By Dan Stanton C 05-Apr-2016 - Last updated on 06-Apr-2016 at 11:03 GMT

### GSK completes \$95m investment for continuous manufacturing in Singapore

By Ben Hargreaves 06-Aug-2019 - Last updated on 06-Aug-2019 at 16:18 GMT



Science of

## Literature on Flow Chemistry, Microreactors and Continuous Processing



Micro Reactors

Chemistry and Engineering



Preparative Chemistry Practical Aspects in Bioprocessing, Nanotechnology, Catalysis and more





Edited by Esther Alza Flow and Microreactor Technology in Medicinal Chemistry













## **General Flow Chemistry Principles**

*The Hitchhiker's Guide to Flow Chemistry*, Seeberger, P. H. et al. *Chem. Rev.* **2017**, 117, 11796





**Anton Paar** 

**3D** Printed

**Reactors** 

www.anton-paar.com

## Typical Flow Reactors (Lab Scale)

### THALESNANO

H-Genie Phoenix Pro www.thalesnano.com



CREAFLOW HANU Reactor www.creaflow.be





**Vapourtec E-Series Flow System** www.vapourtec.com



UNIQSIS

FlowSyn

www.uniqsis.com



Asia System

www.syrris.com



CORNING Advanced Lab Flow Reactor





**Protrix** www.chemtrix.com



EHRFELD Mikrotechnik Lonza FlowPlate Miprowa



## Advantages of Microreactor/Continuous Flow Chemistry

- Very efficient mixing of the reactants (micromixing)
- Rapid heat transfer and temperature control (high surface-to-volume ratio)
- Enhanced mass transfer for multi-phasic reactions (e.g. gas/liquid)
- Control of residence/reaction times
- Hazardous reagents/conditions
- Multi step reactions in a continuous sequence
- Continuous in-line purification possible by:
  - liquid/liquid extraction
  - membrane technology
  - solvent evaporation/swap
- Integrated real-time analytics (PAT)
- Easy scale-up of a proven reaction by:
  - increase of time
  - numbering up (internal, external)
  - sizing up (geometry, length)

Microreactor for Flow Processing



### Scale-Up by Smart Dimensioning

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![](_page_7_Picture_0.jpeg)

## Flow Chemistry in the Kappe Lab – Scalability and Manufacturability (CoG/Sustainability)

Flash Chemistry

![](_page_7_Figure_3.jpeg)

## High-T/p

![](_page_7_Picture_5.jpeg)

Gas-Liquid

![](_page_7_Picture_7.jpeg)

Hazardous Chemistry

![](_page_7_Picture_9.jpeg)

Photochemistry

![](_page_7_Picture_11.jpeg)

Electrochemistry

![](_page_7_Picture_13.jpeg)

Multi-step/APIs

![](_page_7_Picture_15.jpeg)

PAT/Process Control

![](_page_7_Picture_17.jpeg)

![](_page_7_Picture_18.jpeg)

APIs/Intermediates (Clinical Studies and Marketed Drugs) AstraZeneca Lonza AstraZeneca AstraZeneca **Lonza** AstraZeneca AstraZeneca ,Me HO<sub>2</sub>S 0 ОН **PI3K** inhibitors ΗŃ .OMe AZD4573 OPRD 2015 1062 OPRD 2019 2445 CI HO νΟМе HN Me Abediterol Osimertinib Lanabecestat OPRD 2021 947 OPRD 2020 2217 JFC 2017 29, OPRD 2017 878, OPRD 2018 633 Roche Lonza Lonza ASKAT **Patheon** 🔅 Allergan. Μ HO, 'NH RG7774 HN HO OPRD 2021 1206 AAT-076 BAYER Galeterone CEJ 2022 e202200741 X-Ray Imaging F<sub>2</sub>C н ACIE 2014 11557 ÓН Fenebrutinib OPRD 2014 1360 5-HT agonist OPRD 2021 1988 CEJ 2017 176 OH <sub>c</sub>Patheon NHOH Remdesivir/Gilead HO OPRD 2021 1015 NC, "OH OPRD 2020 2362 HO HO ''OH medicines Molnupiravir/Merck for all EJOC 2020 6736 Vilanterol/GSK Vaborbactam Verubecestat/Merck HN-P'''OPh OPRD 2020 2208 Q, `OH CO 2020 24, 7 2018 3133 ACIE 2017 13786 JOANNEUM RESEARCH TU

![](_page_9_Figure_1.jpeg)

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## Flash Chemistry - Synthesis of Epoxides via (Bromomethyl)lithium

![](_page_10_Figure_2.jpeg)

lithiummethane to react with carbonyl compounds to give oxiranes more easily than the corresponding chloroderivative.

LiCH<sub>2</sub>Br however is very unstable and is practically impossible to prepare even at  $-110^{\circ}$ . We tried therefore to prepare it *in situ* in the presence of the carbonyl compound. For this purpose an equimolar solution of 5 $\alpha$ -cholest-3-one and CH<sub>2</sub>Br<sub>2</sub> in THF were treated at  $-78^{\circ}$  with a mole of BuLi in hexane. Work up yielded 20% of the expected oxirane together with the carbinol derived from the direct addition of BuLi to the carbonyl group.

Cainelli, G. et al. *Tetrahedron*, **1971**, *27*, 6109 Michnick, T. J.; Matteson, D. S. *Synlett* **1991**, 631

![](_page_10_Figure_6.jpeg)

## Challenges – Map of Side-Reactions

![](_page_11_Figure_2.jpeg)

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# Plate Reactors (Ehrfeld)

- Lonza FlowPlate
- Very fast reactions (flow rate >1.5 ml/min)
  - Yield affected by heat exchange and mixing
- Plate-type heat exchanger
- Structured mixing channel

![](_page_12_Picture_7.jpeg)

![](_page_12_Picture_8.jpeg)

![](_page_12_Figure_9.jpeg)

![](_page_12_Figure_10.jpeg)

Plouffe, P. et al. Org. Process Res. Dev. 2014, 18, 1286; Plouffe, P. et al. Chem. Eng. J. 2016, 300, 9

![](_page_13_Picture_0.jpeg)

## **Tubing vs Lonza FlowPlate**

-35

-20

![](_page_13_Figure_2.jpeg)

-10

Temp. [°C]

![](_page_13_Picture_3.jpeg)

**TG-Mixer 0.35 mL** Channel width 0.2-0.6 mm Channel depth 0.5 mm

![](_page_13_Figure_5.jpeg)

![](_page_13_Picture_6.jpeg)

## **Tubing vs Lonza FlowPlate**

![](_page_14_Figure_2.jpeg)

![](_page_14_Figure_3.jpeg)

von Keutz, T. et al. Org. Lett. 2019, 21, 10094

![](_page_15_Picture_0.jpeg)

![](_page_15_Figure_1.jpeg)

![](_page_15_Picture_2.jpeg)

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Warran, T. K. et al. *Nature* **2016**, *531*, 381 cf. organolithium method: Siegel, D. et al. *J. Med. Chem.* **2017**, *60*, 1648 (~20% yield)

cf. flow C-glycosylation (Mg): von Keutz, T. et al. Org. Process Res. Dev. 2020, 24, 2362

https://www.gilead.com/purpose/advancing-global-health/covid-19/working-to-supply-remdesivir-for-covid-19 (June 24, 2020) cf. Jarvis, L. M. Scaling up remdesivir amid the coronavirus crisis, *Chem. Eng. News* **2020** (April 20)

![](_page_15_Picture_7.jpeg)

## Key C-Glycosylation Step – Batch Process (0.2 M, -78 °C)

Xue, F. et al. Org. Process Res. Dev. 2020, 24, 1772

![](_page_16_Figure_3.jpeg)

- charge heterocycle (0.845 mol) and anhydrous THF (1.44 L) to oven-dried reactor under N<sub>2</sub> at 20 °C
- 2. stir for **10 min**
- 3. charge BCDMS (1.1 equiv) in THF (360 mL)
- 4. stir for **15 min**
- 5. charge diisopropylamine (1.1 equiv)
- 6. cool to -85 °C to -78 °C (**?? 1 h ??**)
- charge *n*-BuLi (2.5 M in hexane, 1.45 L, 4.3 equiv) within 4 h (-78 °C)
- 8. react for **30 min** (-85 °C to -78 °C)
- 9. charge lactone (2.0 equiv) in anhydrous THF (0.9 L) within 3 h (-85 °C to -78 °C)
- 10. react for **2 h** (-85 °C to -78 °C)
- 11. gradually warm to 0 to 10 °C (?? 1 h ??)
- 12. quench by addition of 1 M citric acid (3.6 L) at <25 °C (**10 min**)
- 13. work-up (62% yield by crystallization)

>12 h (full working day)

![](_page_16_Picture_18.jpeg)

## Key C-Glycosylation Step – Five Stream Flow Procedure (-30 °C)

von Keutz, T. et al. *Org. Process Res. Dev.* **2021**, *25*, 1015

![](_page_17_Figure_3.jpeg)

## Scalability Concept (Smart Dimensioning)

![](_page_18_Figure_1.jpeg)

Roberge, D. M. et al. Chim. Oggi/Chem. Today 2009, 27, 8

![](_page_18_Picture_3.jpeg)

**TU** Graz

**EHRFELD** Mikrotechnik

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## Continuous Nitration Towards Osimertinib Intermediate (Lab Scale)

![](_page_19_Figure_2.jpeg)

## Continuous Nitration Towards Osimertinib Intermediate (Pilot Scale)

![](_page_20_Figure_2.jpeg)

- 0.45 kg/h
- ~11 kg/day

LL-Mixer A5 (11 mL) Channel width 0.5 mm Channel depth 1.25 mm

![](_page_20_Picture_6.jpeg)

- arene/Ac<sub>2</sub>O/H<sub>2</sub>SO<sub>4</sub>/HNO<sub>3</sub> = 1/1.2/1.1/1.1 (mol)
- residence time ~7 s (full mass transfer limited)
- 83% isolated yield (HPLC assay >99%)

Köckinger, M. et al. Org. Process Res. Dev. 2020, 24, 2217

![](_page_20_Picture_11.jpeg)

larger structure of A5 LL-Mixers (~25 mL) width 0.7 mm × depth 1.75 mm (4 × A5 plates in series, ~100 mL)

![](_page_20_Picture_13.jpeg)

## **Process Intensification - Translating Microwave Batch to Flow**

![](_page_21_Figure_1.jpeg)

- transition metal catalyzed C-X bond formation
- other metal-mediated processes
- metathesis, CH-bond activation
- cycloaddition reactions
- rearrangements
- enantioselective reactions
- organocatalysis, biocatalysis
- radical reactions
- oxidations, reductions
- heterocycle synthesis
- total synthesis
- solid- /fluorous phase synthesis
- immobilized reagents, scavengers and catalysts

Camera

solid phase peptide synthesis

Kappe, C. O. Angew. Chem. Int. Ed. **2004**, 43, 6250 (~3300 citations) Kappe, C. O.; Stadler, A.; Dallinger, D. "*Microwaves in Organic and Medicinal Chemistry*" Wiley-VCH, **2005** (2<sup>nd</sup> Ed **2012)** Kappe, C. O. Chem. Rec. **2019**, 19, 15

![](_page_21_Picture_17.jpeg)

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## Why High-T/p Processing? Speeding Up Chemistry (Arrhenius Law)

Batch Microwave 2-Methylbenzimidazol Synthesis

![](_page_22_Figure_3.jpeg)

Temperature [°C]		t >99% conv (HPLC)
CONV	25	9 weeks
CONV	60	5 days
CONV	100	5 h
MW	130 (2 bar)	30 min
MW	160 (4 bar)	10 min
MW	200 (9 bar)	3 min
MW	270 (29 bar)	"1 s"

### Batch Microwave Reactor (300 °C, 30 bar)

![](_page_22_Picture_6.jpeg)

Damm, M. et al. *Org. Process Res. Dev.* **2010**, *14*, 215 cf. essay on microwave effects: Kappe, C. O. et al. *Angew. Chem. Int. Ed.* **2013**, *52*, 1088

![](_page_22_Picture_8.jpeg)

## 

## **Converting Batch Microwave to Continuous Flow Processing**

### Benzimidazole Synthesis

![](_page_23_Figure_3.jpeg)

Damm, M.; Glasnov, T, N.; Kappe, C. O. Org. Process Res. Dev. 2010, 14, 215

![](_page_23_Picture_5.jpeg)

![](_page_23_Picture_6.jpeg)

### Flow Chemistry

*T. N. Glasnov,*\* *C. O. Kappe*\*..... 11956-11968

The Microwave-to-Flow Paradigm: Translating High-Temperature Batch Microwave Chemistry to Scalable Continuous-Flow Processes

![](_page_23_Picture_10.jpeg)

Microwaves not required! Conventionally heated flow reactors (coils or chips) fitted with back-pressure regulators can mimic the high temperatures and pressures attainable in a sealedvessel microwave instrument. Such devices can therefore be used to perform otherwise difficult to scale microwave chemistry (see scheme).

![](_page_23_Picture_13.jpeg)

Glasnov, T.; Kappe, C. O. *Chem. Eur. J.* **2011**, *17*, 11956

## Accessing "Forbidden" (and "Forgotten") Chemistries

![](_page_24_Figure_2.jpeg)

## More High-T/p Flow Chemistry (Lab Scale)

### Newman-Kwart Rearrangement

![](_page_25_Figure_3.jpeg)

Eur. J. Org Chem. 2009, 1321

### **Diels-Alder Reactions**

![](_page_25_Figure_6.jpeg)

### Claisen Rearrangement

![](_page_25_Figure_8.jpeg)

### Methylations Using Dimethylcarbonate

![](_page_25_Figure_10.jpeg)

Green Chem. 2012, 14, 3071

### Fischer Indole Synthesis

![](_page_25_Figure_13.jpeg)

\_\_\_\_\_

![](_page_25_Figure_15.jpeg)

## Tetrazole Synthesis in Flow under High-T/p Conditions

Sartans (Angiotensin II Receptor Antagonists)

![](_page_26_Figure_3.jpeg)

### Two-Feed Continuous Flow Approach (In Situ HN<sub>3</sub>)

![](_page_26_Figure_5.jpeg)

Gutmann, B. et al. *Angew. Chem. Int. Ed.* **2010**, *49*, 7101; *J. Flow Chem.* **2012**, *2*, 8 Mechanism: Cantilo, D. et al. *J. Org. Chem.* **2012**, *77*, 10882; *J. Am. Chem. Soc.* **2011**, *133*, 4465

![](_page_26_Picture_7.jpeg)

Tetrazole Synthesis in Flow under High-T/p Conditions

### Cannabinoid Receptor 2 (CB2) Agonist (RG7774)

- Microwave batch to flow translation
- Process analytics in real time (NMR/FT-IR)
- Continuous flow synthesis and workup strategy (~80% yield after crystallization, 10 g/h productivity)

![](_page_27_Figure_5.jpeg)

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![](_page_27_Figure_6.jpeg)

*i*PrOAc at 0 °C

Sagmeister, P. et al. Org. Process Res. Dev. 2021, 25, 1206 cf. microwave batch procedure: Chandgude, A. L.; Dömling, A. Eur. J. Org. Chem. 2016, 2383

![](_page_27_Figure_9.jpeg)

Tetrazole Synthesis in Flow under High-T/p Conditions

### Cannabinoid Receptor 2 (CB2) Agonist (RG7774)

- Microwave batch to flow translation
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![](_page_28_Figure_5.jpeg)

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![](_page_28_Figure_6.jpeg)

Sagmeister, P. et al. Org. Process Res. Dev. 2021, 25, 1206 cf. microwave batch procedure: Chandgude, A. L.; Dömling, A. Eur. J. Org. Chem. 2016, 2383

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# Scaling-up Gas-liquid Reactions in Batch – Mass Transfer Limitations

![](_page_29_Picture_2.jpeg)

Volume (mL)	5	25	50	100	250
Radius r (m)	0.014	0.021	0.025	0.033	0.043
Interfacial area a (m <sup>2</sup> m <sup>-3</sup> )	107	71	60	46	35

Review: Mallia, C. J.; Baxendale, I. R. Org. Process Res. Dev. 2016, 20, 327

![](_page_30_Picture_0.jpeg)

## Mass Transport Intensification in Flow

Gas-Liquid Flow Regimes - Interfacial Areas

- interfacial area in coil reactors is 50 to 700 m<sup>2</sup>m<sup>-3</sup>
- interfacial area in micoreactors up to 18.000 m<sup>2</sup>m<sup>-3</sup>

Mallia, C. J.; Baxendale, I. R. *Org. Process Res. Dev.* **2016**, *20*, 327 Yue, J. et al. *Chem. Eng. Sci.* **2007**, *62*, 2096

![](_page_30_Figure_6.jpeg)

### **Other Factors**

- higher solubility of gases in pressurized reactors (Henry's law)
- exact dosing using mass flow controllers, use of large stoichiometric excess (headspace) avoided
- safety aspects

Gavriilidis, A. et al. *React. Chem. Eng.* **2016**, *1*, 595; Pieber, B.; Kappe, C. O. *Top. Organomet. Chem.* **2016**, *57*, 97 Hone, C. A.; Kappe, C. O. *Top. Curr. Chem.* **2019**, *377*, 2; Kockmann, N. et al. *React. Chem. Eng.* **2017**, *2*, 258

![](_page_30_Picture_12.jpeg)

## **Ozone Chemistry in Microreactors**

## Lonza

### Switching Quench Inlets

![](_page_31_Figure_3.jpeg)

Intensive gas-liquid mixing

Polterauer, D. et. al. *React. Chem. Eng.* **2021**, *6*, 2253 cf. flow ozonolysis in tubing (22 s): Irfan, M. et al. *Org. Lett.* **2011**, *14*, 984

![](_page_31_Figure_6.jpeg)

## Continuous Flow Approaches to the Abediterol Side Chain

### Original Batch Procedure (Almirall)

![](_page_32_Figure_3.jpeg)

![](_page_32_Picture_4.jpeg)

![](_page_32_Figure_5.jpeg)

very high potency β2-adrenoceptor agonist (kg demand)

Duran Puig, C. et al. (Almirall) WO2006/122788

![](_page_32_Picture_8.jpeg)

## Continuous Flow Approaches to the Abediterol Side Chain

### Alternative Batch Procedure (AstraZeneca)

![](_page_33_Figure_3.jpeg)

Munday, R. H. et al. (AstraZeneca) Tetrahedron Lett. 2019, 60, 606

![](_page_33_Picture_5.jpeg)

## Continuous Flow Approaches to the Abediterol Side Chain

### "Telescoped" Flow Procedure

![](_page_34_Figure_3.jpeg)

Prieschl, M. et al. *Green Chem.* **2020**, *22*, 5762 (step 1) García-Lacuna, J. et al. *Org. Process Res. Dev.* **2021**, *25*, 947 (steps 2-4)

![](_page_34_Picture_5.jpeg)

## **Continuous Flow Photochemistry**

### Advantages of Light-Induced Reactions

- clean and safe method of activation
- economical
- generates complexity otherwise difficult to obtain
- but: difficult to scale (Beer-Lambert Law)

### Flow Photochemistry

![](_page_35_Figure_7.jpeg)

![](_page_35_Figure_8.jpeg)

- uniform irradiation
- accurately controlled exposure time (flow rate)
- small amounts of solvent near to lamp (safe)
- scalable
- Reviews: Politano, F.; Oksdath-Mansilla, G. *Org. Process Res. Dev.* 2018, 22, 1045
  Cambie, D. et al. *Chem. Rev.* 2016, *116*, 10276; Buglioni, L. et al. *Chem. Rev.* 2022, *122*, 2752
  Elliott, L. D. et al. *Chem. Eur. J.* 2014, *20*, 15226; Bonfield, H. E. et al. *Nat. Comm.* 2020, *11*, 804
  Booker-Milburn, K. I. et al. *Beilstein J. Org. Chem.* 2012, *8*, 2025

![](_page_35_Picture_14.jpeg)

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## Building Capability: 10 Years of Flow Photochemistry in the Kappe Group

### Home-Built Reactors

![](_page_36_Picture_3.jpeg)

since 2013

- large selection of light sources (CFL, LEDs, blacklight)
- simple and versatile

### Vapourtec UV150

![](_page_36_Picture_8.jpeg)

since 2015

- tubing-based reactor
- LEDs and medium pressure Hg lamp

### Corning Advanced-Flow Lab Photo Reactor

![](_page_36_Picture_13.jpeg)

since 2018

- plate-based reactor
- LED arrays with a choice of 12 wavelengths

Combined capability to cover the whole spectrum of UV and visible photochemical transformations

![](_page_36_Picture_18.jpeg)

## Corning<sup>®</sup> Advanced-Flow<sup>™</sup> Photo Reactor – Lab Scale

![](_page_37_Figure_2.jpeg)

- Small channel depth for effective irradiation
- Mixing structure for multiphasic reactions
- Improved temperature control
- Tuneable wavelength and intensity

- a) Huber thermostat (reactor plate temp. control)
- b) Control module
  - HPLC pumps
  - mass flow controller (gases)
  - thermostat control
  - system parameter monitor
- c) Reactor (2.8 mL) and LED housing
- d) Thermostat (LED plate temp. control)
- e) Lamp control module

NBS Benzylic Bromination Chen, Y. et al. *ChemPhotoChem* **2018**, *2*, 906 Ethylene [2+2] Williams, J. D. et al. *Org. Process Res. Dev.* **2019**, *23*, 78 Nitrosyl Chloride Lebl, R. et al. *React. Chem. Eng.* **2019**, *4*, 738 Catalyst-free ATRA Rosso, C. et al. *Org. Lett.* **2019**, *21*, 5341 Reduction of Ar-X Steiner, A. et al. *Eur. J. Org. Chem.* **2019**, 5807 ATRA Steiner, A. et al. *React. Chem. Eng.* **2021**, *6*, 2434

![](_page_38_Picture_0.jpeg)

## Iodoperfluoroalkylation of Alkenes (ATRA)

![](_page_38_Figure_2.jpeg)

Wavelength	Yield [%]
365 nm	95
385 nm	97
405 nm	97
422 nm	95
450 nm	95
540 nm	88
610 nm	0

![](_page_38_Picture_5.jpeg)

## Iodoperfluoroalkylation of Alkenes (ATRA)

![](_page_39_Figure_1.jpeg)

![](_page_39_Picture_2.jpeg)

Wavelength	Yield [%]
365 nm	95
385 nm	97
405 nm	97
422 nm	95
450 nm	95
540 nm	88
610 nm	0

Wavelength	Yield [%]
365 nm	94
385 nm	94
405 nm	94
422 nm	34
450 nm	0
540 nm	0
610 nm	0

![](_page_39_Picture_5.jpeg)

![](_page_39_Picture_6.jpeg)

## Iodoperfluoroalkylation of Alkenes (ATRA)

![](_page_40_Figure_2.jpeg)

Continuous Benzylic Bromination – Lab Scale with Quench in Flow

### 2,6-Dichlorobenzylbromide (API Intermediate)

![](_page_41_Figure_2.jpeg)

cf. BrCN/Br<sub>2</sub> generator: Glotz, G. et al. *Angew. Chem. Int. Ed.* **2017**, *56*, 13786 Steiner, A. et al. *Green Chem.* **2020**, *22*, 448

![](_page_41_Picture_4.jpeg)

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![](_page_42_Figure_0.jpeg)

Steiner, A. et al. Org. Process Res. Dev. 2020, 24, 2208

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# HANU Reactor – Handling Solids in Flow

Pilot Scale Reactor (150 mL)

![](_page_43_Picture_3.jpeg)

![](_page_43_Picture_4.jpeg)

![](_page_43_Picture_5.jpeg)

![](_page_43_Picture_6.jpeg)

## Dual Nickel/Photocatalytic C-N Cross-couplings

### Iridium Complexes as Photocatalysts (Buchwald, MacMillan)

![](_page_44_Figure_2.jpeg)

![](_page_44_Figure_3.jpeg)

### Carbon Nitrides as Photocatalysts (Antonietti, König, Pieber)

![](_page_44_Figure_5.jpeg)

Gosh, I. et al. *Science* **2019**, *365*, 360 cf. Pieber, B. et al. *Nature Catal.* **2020**, *3*, 611; *Angew. Chem. Int. Ed.* **2019**, *58*, 9575

![](_page_44_Picture_7.jpeg)

Iridium photocatalyst Ir[dF(CF<sub>3</sub>)ppy]<sub>2</sub>(dtbbpy)PF<sub>6</sub> 800 €/g Sigma-Aldrich

![](_page_44_Picture_9.jpeg)

![](_page_44_Picture_10.jpeg)

CCFLOW

mpg-CN inexpensive, solid, recycable

## Semi-heterogeneous Photoredox Catalysis in the HANU Reactor

,CO₂Et

![](_page_45_Figure_2.jpeg)

![](_page_45_Figure_3.jpeg)

Pulsation characteristics optimized for narrow RTD 

![](_page_45_Figure_5.jpeg)

Rosso, C. et al. React. Chem. Eng. 2020, 5, 597

## Electroorganic Synthesis – A Renaissance

### Book

 Hammerich, O.; Speiser B. Organic Electrochemistry: Fifth Edition; CRC Press: Boca Raton, 2016

![](_page_46_Picture_3.jpeg)

![](_page_46_Picture_4.jpeg)

## Electroorganic Synthesis – Advantages and Opportunities

### Sustainable and Cost-Efficient

VS

![](_page_47_Picture_3.jpeg)

![](_page_47_Picture_4.jpeg)

KMnO<sub>4</sub> 1-2 €/mol LiAlH<sub>4</sub> 8 €/mol mCPBA 7 €/mol

![](_page_47_Figure_6.jpeg)

![](_page_47_Figure_7.jpeg)

Enabling

![](_page_48_Picture_0.jpeg)

![](_page_48_Figure_1.jpeg)

## Common Opioid N-Demethylation Methods

![](_page_49_Figure_2.jpeg)

![](_page_50_Picture_0.jpeg)

## **Continuous Manufacturing of Opioid Derived APIs**

Pd-Catalyzed Aerobic N-Demethylation

![](_page_50_Figure_3.jpeg)

WO 2017184979, WO 2017185004

Gutmann, B. et al. Chem. Eur. J. **2016**, 22, 10393; ACS Sust. Chem. Eng. **2016**, 4, 6048; Eur. J. Org. Chem. **2017**, 914 Eur. J. Org. Chem. **2017**, 6505

![](_page_50_Picture_6.jpeg)

![](_page_51_Picture_0.jpeg)

## Electrochemical N-Demethylation of Oxycodone

![](_page_51_Figure_2.jpeg)

Jud, W. et al. Chem. Methods 2021, 1, 36

## Electrochemical N-Demethylation of Oxycodone

![](_page_52_Picture_1.jpeg)

Sommer, F. et al. ACS Sustain. Chem. Eng. 2022, 10, 8988

![](_page_52_Picture_3.jpeg)

## **Comparison of Conventional and Electrochemical Procedures**

	EtOCOCI	Electrochemical A	Electrochemical B
Type of reaction	Stochiometric Reagent	Electricity (Et <sub>4</sub> NBF <sub>4</sub> )	Electricity (KOAc)
T [°C]	60	rt	rt
Workup	Extraction	Chromatography	Extraction
Solvent	CHCl <sub>3</sub>	MeCN/MeOH	EtOH
Yield [%]	60	89	98
Quench	50 L H <sub>2</sub> O/kg oxycodone	-	-
Atom Economy	12	35	81
PMI (without solvent)	3.5	2.9	1.2
РМІ	37	62	15
EcoScale	49	60	90

![](_page_53_Picture_3.jpeg)

## Immobilized Organocatalysts for Chiral API Synthesis

Asymmetric Conjugate Addition nstitut In collaboration with Català d'Investigació M. A. Pericas at ICIQ, Spain Química 10 bar NEN Ph Ph СНО. PS NH ÓTBS 60 °C ,COOMe 20 min ĊOOMe ,СНО Paroxetine (SSRI) 7 h collection time (1 equiv.) COOMe 17.26 g (84% yield) AcOH (0.6 equiv) COOMe 2.47 g h<sup>-1</sup> 0.07 mL min<sup>-1</sup> (2 equiv.) 97% ee (E-factor: 0.7) neat Flow organocatalysis under solvent-free conditions 7-h long experiment under optimum flow conditions Isolation of analytically pure product by evaporation 

Ötvös, S. et al. *Chem. Sci.* **2019**, *10*, 11141 Review: Ötvös, S.; Kappe, C. O. *Green Chem.* **2021**, *23*, 6117

![](_page_54_Picture_3.jpeg)

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## Telescoped Reductive Amination–Lactamization–Amide/Ester Reduction

![](_page_55_Figure_2.jpeg)

Ötvös, S. et al. Chem. Sci. 2019, 10, 11141; ChemSusChem 2020, 13, 1800; Org. Lett. 2022, 24, 1066

**Telescoped Synthesis of Agrochemical Intermediate** Me<sub>2</sub>N Me<sub>2</sub>N "Trifludimoxazin" (BASF) NH<sub>2</sub> O<sub>2</sub>N NO<sub>2</sub> H2N water diamino, intermediate dinitro intermediate (quench) Steinbrenner, U. et al. Me<sub>2</sub>N (air/light sensitive) (explosive) WO 2015071087 A1, 2015 aq waste neat 60 °C, 20 min  $H_2$ 18 bar liquid/liquid BPR separator 2 min  $NH_2$ Pd/C n glass 0°C AF2400 100% HNO<sub>3</sub> 80 °C static toluene H<sub>2</sub> in 20% oleum mixer 5 min **Batch Process (Patent)** 2.5 equiv methanol 86% (90% purity) **H-Cube Pro** (co-solvent) overall ~67% 37% HCI **Continuous Process** 1.2 equiv overall >80% BASE Quench -Nitration The Chemical Compan Phase Hydrogenation Gas Cyclization Liquid/liquid separation release extraction EP 15201920.4

Cantillo, D. et al. Org. Process Res. Dev. 2017, 21, 125

![](_page_56_Picture_2.jpeg)

Lab of the Future: Integration of Multiple Types of PAT Tools to a Single Platform

![](_page_57_Picture_2.jpeg)

**Mass Flow** Control **Reactant 2 Cascade Mixer** Reactant 1 Reactant 2 **Reactant 1** Outlet BROOKS ReactIR Capillary Probe Reactor thermostat  $\leq$ Heat Exchanger IR **T2** Lonza FlowPlate JUUUC LAB 0 Reactant 3 Temperature EHRFELD Mikrotechnik **Pressure Probes Reactant 3 Probes** JOANNEUM RESEARCH https://ehrfeld.com/en/products/mmrs.html TU

Laboratory of the Future: A Modular Flow Platform with Multiple Integrated PAT Tools for Multistep Reactions

![](_page_59_Figure_1.jpeg)

Sagmeister, P. et al. React. Chem. Eng. 2019, 3, 1571

![](_page_59_Picture_3.jpeg)

## Model-based Strategies for Real-time Control of API Synthesis

![](_page_60_Figure_2.jpeg)

## Autonomous Continuous Flow Chemistry Platform

![](_page_61_Figure_1.jpeg)

![](_page_62_Picture_0.jpeg)

## GSK Continuous API Manufacturing (Singapore)

![](_page_62_Picture_2.jpeg)

Allford, G.; Hagger, B. 7<sup>th</sup> Symposium on Continuous Flow Reactor Technology for Industrial Applications, Delft, Netherlands, Sept 29-Oct 1, **2015** See also: Roberts, K. Chemistry and Industry Magazine **2016** (6), p. 31-33

![](_page_63_Picture_0.jpeg)

## End-to-End Continuous Manufacturing (MIT)

### Novartis CM Facility (Basel)

![](_page_63_Picture_3.jpeg)

Mullin, R. Chem. Eng. News 2019, 97 (17), p. 28

### Pharmacy on Demand (DARPA)

![](_page_63_Picture_6.jpeg)

Adamo, A. et al. *Science* **2016**, *352*, 61 Zhang, P. et al. *Chem. Eur. J.* **2018**, *24*, 2776 cf. Coley, C. et al. *Science* **2019**, *365*, Issue 6453, eaax1566

## **Conclusions – Continuous Processing and Flow Chemistry**

- Safer, more robust (in-line PAT) and scalable processes
- New chemistries ("designer reagents") and processing windows in fit-for-purpose reactors
- Allows redesigning of APIs syntheses utilizing "forbidden" chemistries
- Cheaper and more sustainable access to APIs and essential medicines (on-site, on-demand)

![](_page_64_Picture_6.jpeg)

![](_page_64_Picture_7.jpeg)

Novartis Continuous Manufacturing Lab (2018)

![](_page_64_Picture_9.jpeg)

![](_page_65_Picture_0.jpeg)

## Acknowledgements: CCFLOW Team and Funding Agencies

Center for Continuous Flow Synthesis and Processing (http://ccflow.at)

![](_page_66_Picture_2.jpeg)

![](_page_66_Picture_3.jpeg)

![](_page_66_Picture_4.jpeg)


![](_page_66_Picture_6.jpeg)

![](_page_66_Picture_7.jpeg)

Der Wissenschaftsfonds.

![](_page_66_Picture_8.jpeg)

![](_page_66_Picture_9.jpeg)

![](_page_66_Picture_10.jpeg)

![](_page_66_Picture_11.jpeg)